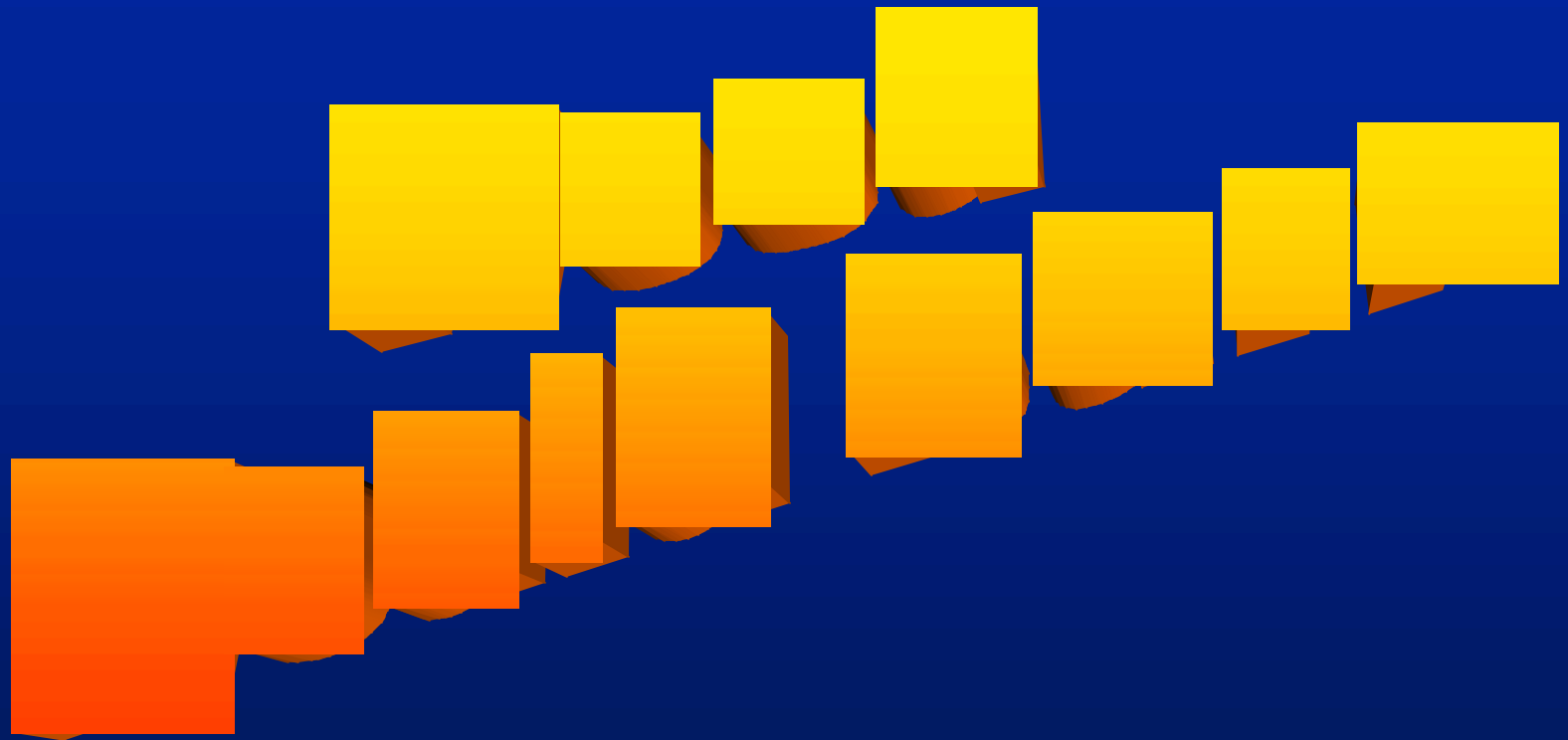




**British French - French Flame Joint Meeting  
Lille 9/10 March 2009**



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Energy and Environment Engineering, Sheffield University**



# **Presentation Outline**

- **Energy, Environment and Sustainability**

- Wood Fuel: (experiments show less particulate emissions than coal)
- High moisture  $\Rightarrow$  Condensing boiler (CHP)

- **Power generation  $\Rightarrow$  High Pressure Combustion**

- 80bars – condense moisture  $> 200^{\circ}\text{C}$  hence recover energy for power
- 80bars – ‘condense’  $\text{CO}_2 > 30^{\circ}\text{C}$ ,  $\Rightarrow$  sequestration of ‘liquid’  $\text{CO}_2$
- 80bars – low superheater stress  $\Rightarrow$  Higher temperature and efficiency
- Liquid oxygen – pump to high pressure

- **Fluidized bed**

- Wood chip slurry fuel - pump to high pressure
- Water moderates oxy-fuel flame temperature
- Hydrogen from water-gas reaction  $\Rightarrow$  Ultra-superheated steam
- Steam turbine entry temperature  $1000^{\circ}\text{C}$  to  $1400^{\circ}\text{C}$
- Overall electrical power generation efficiency  $> 60\%$  possible

- **Conclusion: System removes  $\text{CO}_2$  from the atmosphere!!**

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# Properties of coal, wood and RDF samples

		Coal	White Oak	Pine bark	RDF
Proximate analysis (%)	Fixed Carbon	55.8	17.2	33.9	9.8
	Volatiles	33.9	81.3	54.7	67.6
	Ash	10.3	1.5	0.4	18.9
Ultimate analysis (% daf)	C	84.2	50.2	56.5	61.2
	H	5.6	5.5	5.6	8.2
	O	5.5	43.8	37.9	26.6
	N	1.3	0.4	0.0	1.3
	S	3.5	0.0	0.0	0.2
HHV (MJ/kg) DRY!		31.75	19.42	21.78	22.3

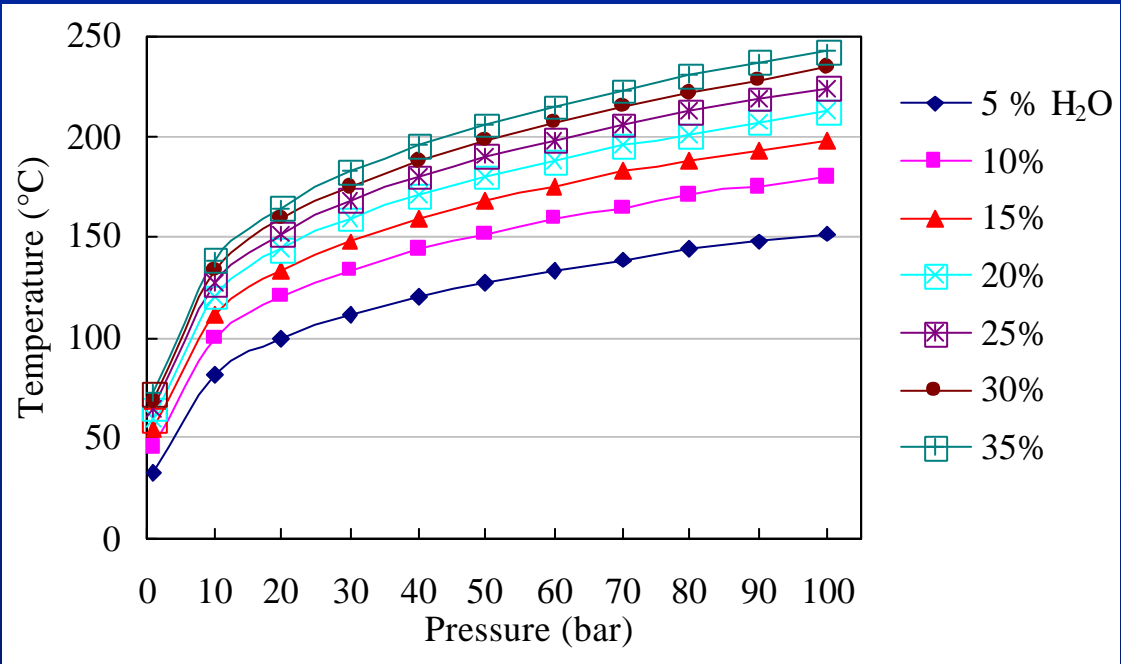
**But:** Raw wood contains 60% moisture and combustion products include water.  
Each 10% moisture reduces heating value by 2MJ/kg  
Thus raw wood heating value is typically ~8MJ/kg.

**Therefore:**

**Use low grade waste industrial heat to “add value” to wood by drying**

# **Condensing Boilers**

- **CHP** – Sheffield is lead city in the UK. Current district heating return water temperature is  $\sim 70^{\circ}\text{C}$
- **Condensing boilers recover latent heat of water in the flue gas**
  - Atmospheric pressure condensation temperature is  $\sim 55^{\circ}\text{C}$
  - Hence require return building heating water at  $30^{\circ}\text{C}$  using large radiators or under-floor heating in order to recover the latent heat energy
- **Alternatively; Dew point increases with pressure**
  - Use high pressure combustion to raise dew point to more than  $200^{\circ}\text{C}$
  - Large amount of heat recovered at this high temperature can be recycled into power generation by:
    - » Heating boiler feed water,
    - » Heating combustion air or oxygen
    - » etc

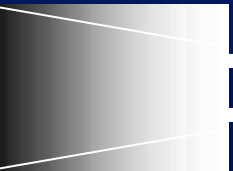
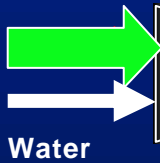


**Flue gas dew point temperature  
as a function of pressure and  
moisture content**

**Hi-Efficient Biomass/Coal Power Generation with Latent Heat Recovery and CO2 Sequestration**

CO<sub>2</sub>, H<sub>2</sub>O, CO, H<sub>2</sub>  
Trace: N<sub>2</sub>, fly ash, HCl, H<sub>2</sub>S, COS  
at ~850°C 80bars

**Wood chips**



Air

O<sub>2</sub>

N<sub>2</sub>

GCR = Gas cleaning residues

Ash

80bars



O<sub>2</sub>

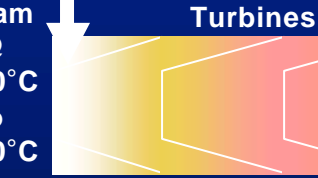
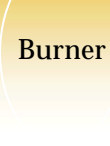
O<sub>2</sub>

H<sub>2</sub>

Steam @ 1200°C to 1400°C at ~80bars

Pressure Balanced UHx Heat Exchanger

~1100°C  
Steam @ 900°C to 1000°C



Air (Optional district heat)

N<sub>2</sub>

Heat Exchanger

Generator

Power ?~60%

Latent Heat Recovery



CO  
N<sub>2</sub>  
GCR  
H<sub>2</sub>O

'Liquid' CO<sub>2</sub> to Sequestration at 80bars

Water pump

2°C, 0.005bar

# **High Pressure (>80bars) Combustion of Wood**

## ● **Pressurised Combustor Technologies**

- Moving Grate
- Entrained pulverised fuel jet
- Shaft combustor
- Rotary kiln
- Circulating fluid bed
- Bubbling fluid bed \*\*\* (preferred technology)

## ● **Fuel feeding**

- Wood slurry pump (liquid, therefore high efficiency)
- Drain surplus water, but wet wood is OK

## ● **Bed temperature control**

- Heat load, fuel-oxygen ratio, **flue gas CO<sub>2</sub> recycle, or Water**
- Large heat recovery at high temperature is recycled into power generation

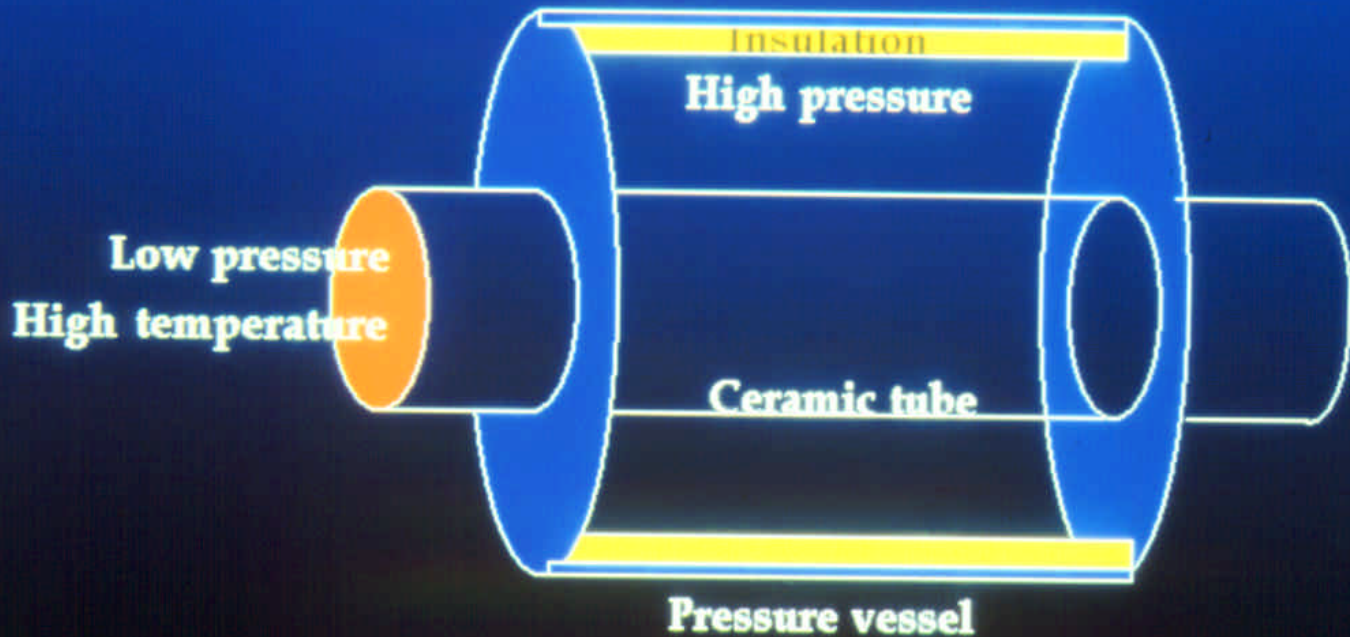
## ● **Hydrogen generation**

- Water increases hydrogen production by water-gas reaction

# ***High Pressure Combustion of Wood***

- **Pressurised System Heat Transfer**
  - Radiation increases with pressure
  - Convection increases faster with pressure
  - Heat transfer areas are much smaller
  - 500MW power plant CO<sub>2</sub> exhaust pipe is ~30cm diameter
- **Pressurised Bubbling Fluidised Bed**
  - Contained in pressure vessel insulated on inside
- **Gas Cleaning**
  - Particles removed in high temperature heat recovery condenser
  - Scrubbers small as gas density is very high
  - Carbon dioxide recovery directly as supercritical 'liquid' at this pressure
- **High temperature technology**
  - Heat transfer tubes are in **compression**
  - Ceramic heat exchangers >1000°C

# *UHX Heat Exchanger Principle*



A Plate Heat Exchanger could be used with balanced pressures!

# UHX Heat Exchanger (70kW)

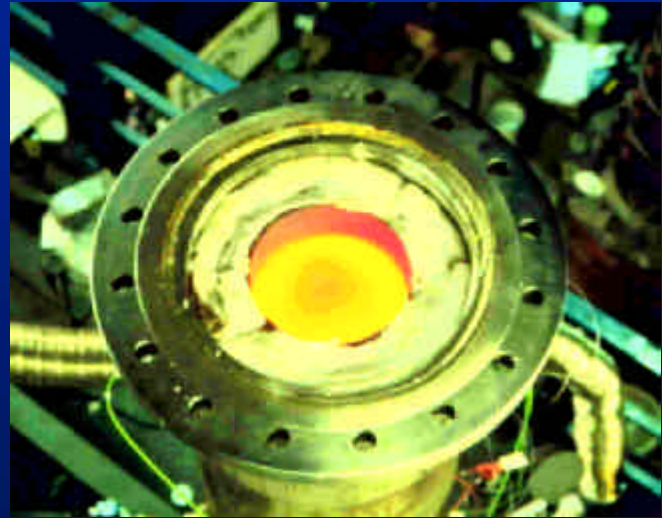


Fig.7

# ***Gas Cleaning***

- **Contaminants change the dew point for water condensation**
- **‘Liquid’ carbon dioxide recovery by ‘condensation’ at atmospheric pressure!**
- **Contaminants also change the ‘dew point’ for CO<sub>2</sub> condensation**
- **Must carry out exact calculations for condensations**





- Andersen probe and particle sample photos

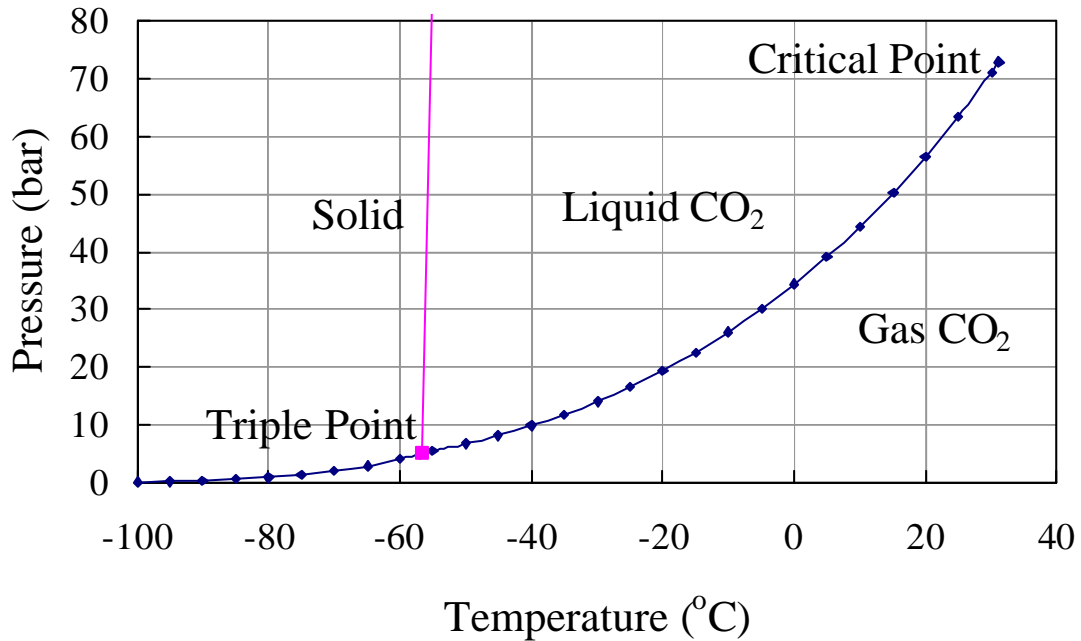


Andersen Probe



Particle sample plate






**Phase diagram for pure carbon dioxide**

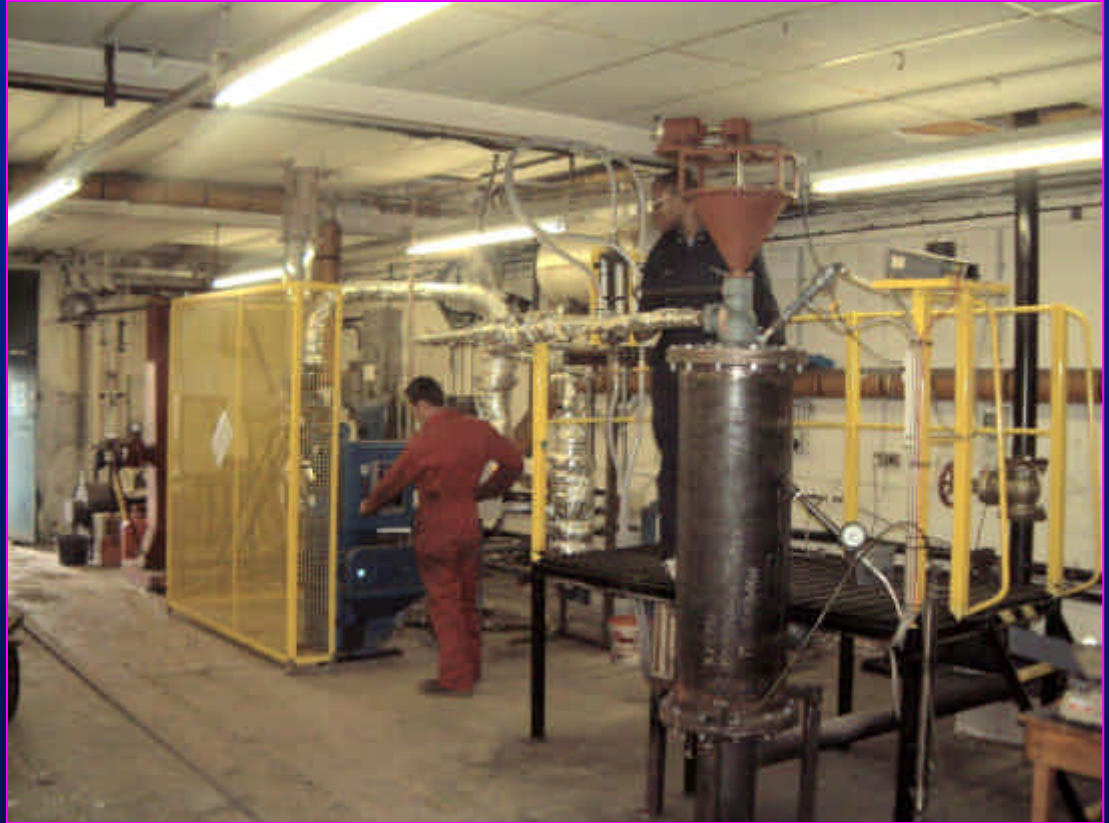
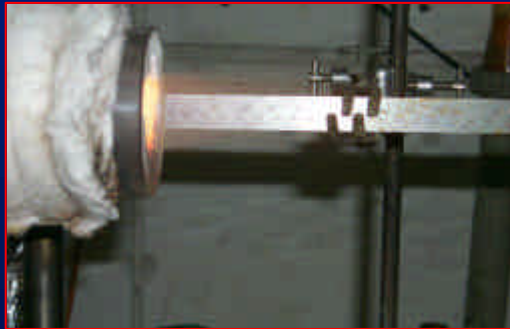


- **High temperature technology**

- Ceramic heat exchangers  $>1000^{\circ}\text{C}$
  - Burn hydrogen-oxygen in steam to raise its temperature to  $1400^{\circ}\text{C}$
  - Efficient steam turbine engine cycle with cooled turbine blades
- 

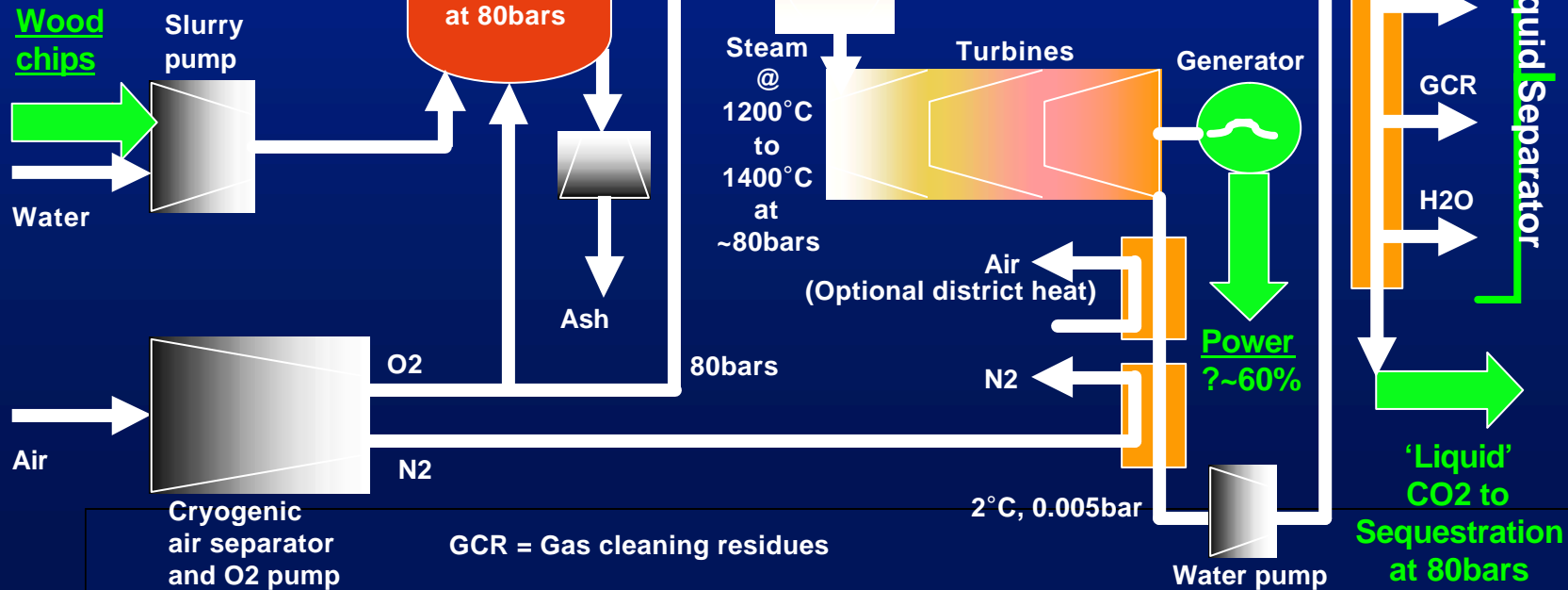
# **Ultra Superheated Steam**

Steam at 1600°C



**Hi-Efficient Biomass/Coal Power Generation with Latent Heat Recovery and CO2 Sequestration**

CO<sub>2</sub>, H<sub>2</sub>O, CO, H<sub>2</sub>  
Trace: N<sub>2</sub>, fly ash, HCl, H<sub>2</sub>S, COS  
at ~850°C 80bars



# **Conclusions**

- **Decarbonise the atmosphere with advanced wood burning technology**
  - **Particles emitted by wood combustion for CHP must be controlled**
  - **Moisture in Wood:** Dry wood using low grade heat, or condense after combustion to recover latent heat of water
  - **Burn and Condense at High Pressure:** Recovers latent heat  $>200^{\circ}\text{C}$  for energy generation and allows 'condensation' of  $\text{CO}_2$  for sequestration; Pump liquid wood chip slurry efficiently to high pressure; Inverted heat transfer tube stress (compression) allows advanced materials.
  - **Oxy-fuel Combustion:** Control flame temperature with water (forms  $\text{H}_2$  by water-gas reaction) or recycled  $\text{CO}_2$ . Pump oxygen as liquid to high pressure.
  - **Raise power generation efficiency for biomass and/or coal fuel  $> 60\%$  by oxy-hydrogen superheating steam to  $\sim 1400^{\circ}\text{C}$**
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